# **IONOSCIC**<sup>®</sup>

Minimizing risk. Maximizing potential.®

13<sup>th</sup> December 2023 2023 EPSC – Third European Conference On Plant & Process Safety – Maastricht, Netherlands **Dynamic Vapor Breakthrough: Avoiding Pitfalls for ERS Design** 

Daniel Wilkes, Consultant wilkes.d.uk@iomosaic.com

QMS 7.3 7.4.F13 Rev.3

© ioMosaic Corporation

Any information contained in this document is copyrighted, proprietary, and confidential in nature belonging exclusively to ioMosaic Corporation. Any reproduction, circulation, or redistribution is strictly prohibited without explicit written permission of ioMosaic Corporation.





## **Daniel Wilkes, AMIChemE – Consultant** ioMosaic Corporation UK Office

- Masters in Chemical Engineering (University of Bath, UK)
  - Molecular dynamics research for drug molecule characterization
- Industrial experience
  - Process dynamics, fluid mechanics and mathematical modelling
  - Reaction engineering and modeling runaway reactions
  - Relief systems design for reactive systems
  - Relief device stability analysis
  - Deflagration modelling
  - Guest lecturing 'Pressure Relief Engineering' at the University of Bath, UK
  - Management of capital engineering projects
- Contact info: wilkes.d.uk@iomosaic.com





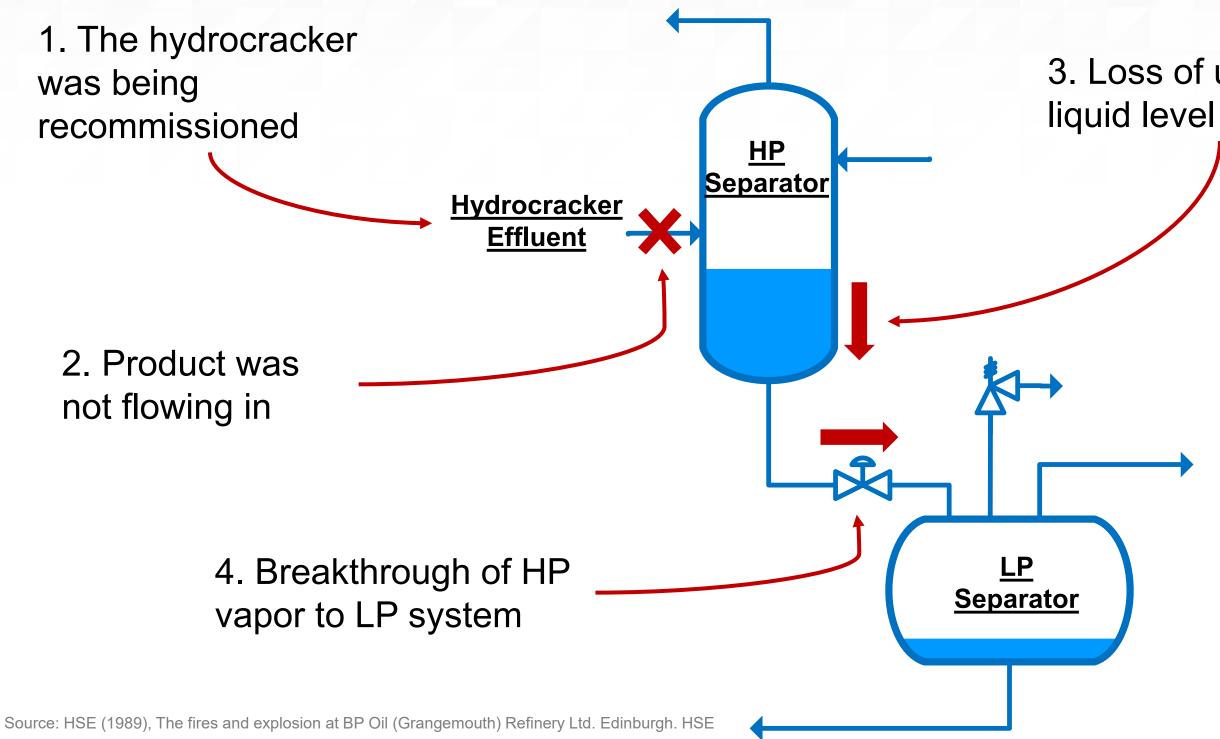
#### **Table of Contents**

- 1 What is vapor breakthrough?
- 2 Steady state relief system sizing methodologies for vapor breakthrough
- 3 Additional considerations for steady state methods
- 4 Rigorous dynamic modelling of vapor breakthrough
- 5 Dynamic simulation results
- 6 Conclusions





**Case Study: Grangemouth Hydrocracker Explosion and Fire (22nd March 1987)** 



Source: Wikipedia: Grangemouth Refinery

3. Loss of upstream

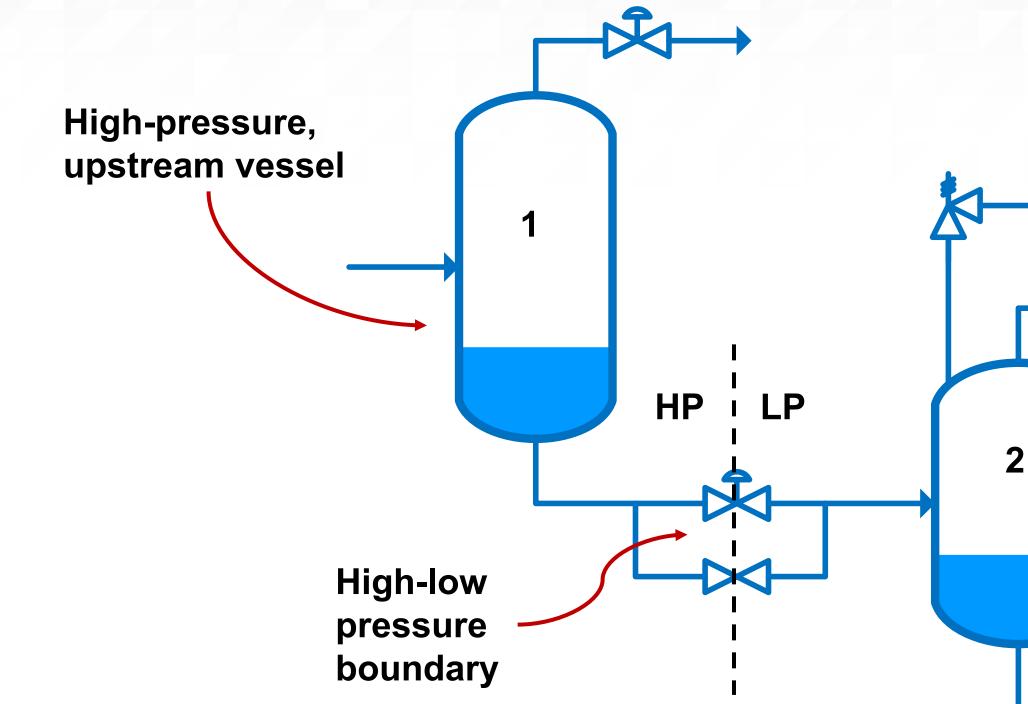


#### **Design Issues:**

- Pressure relief valve had been sized for fire
  - Low-level trip on the HP separator liquid level was credited to prevent breakthrough, but operators had disabled it



### Vapor breakthrough may occur if the liquid seal is lost between a high-pressure and lowpressure system

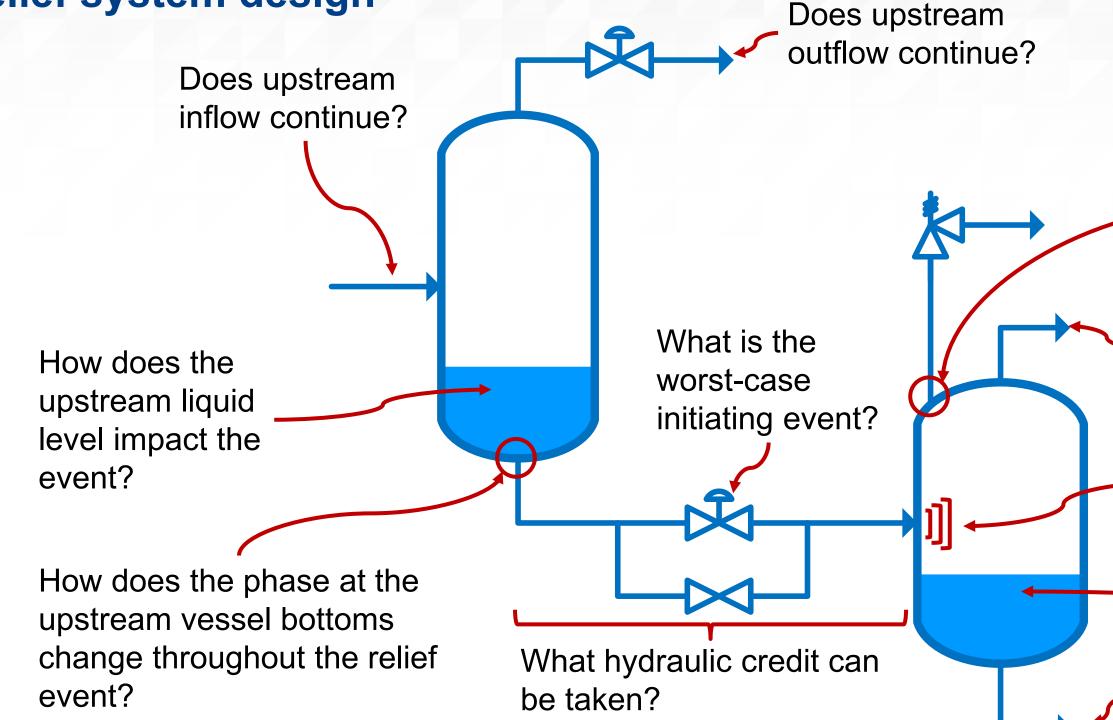


Source: ioMosaic Corporation

Low-pressure, - downstream vessel



### Vapor breakthrough is a complex, dynamic scenario with many elements to consider in relief system design



Source: ioMosaic Corporation

What is the fluid phase at the relief system inlet piping?

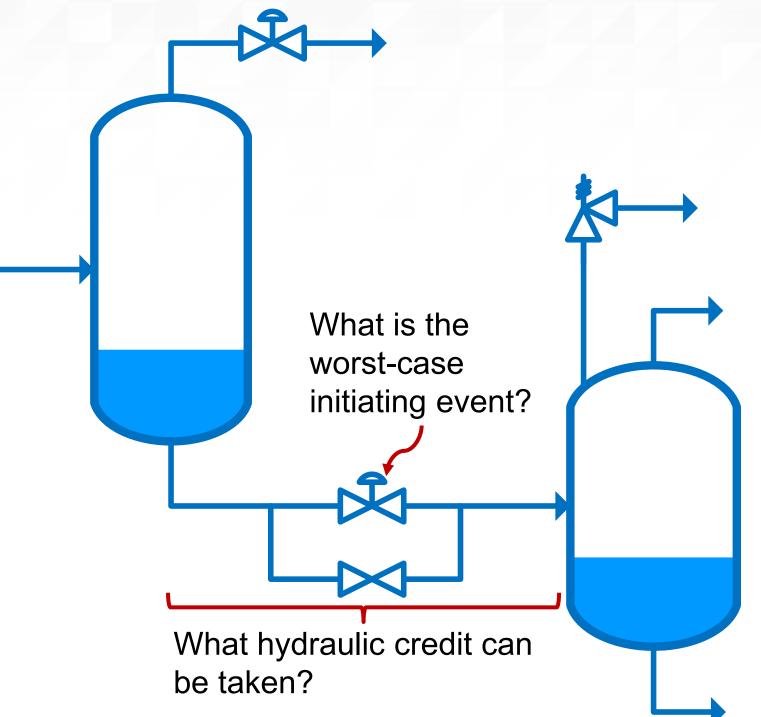
Does downstream vapor outflow continue?

Could high pressure surges occur downstream?

Does downstream liquid outflow continue? How does the downstream liquid level impact the event?



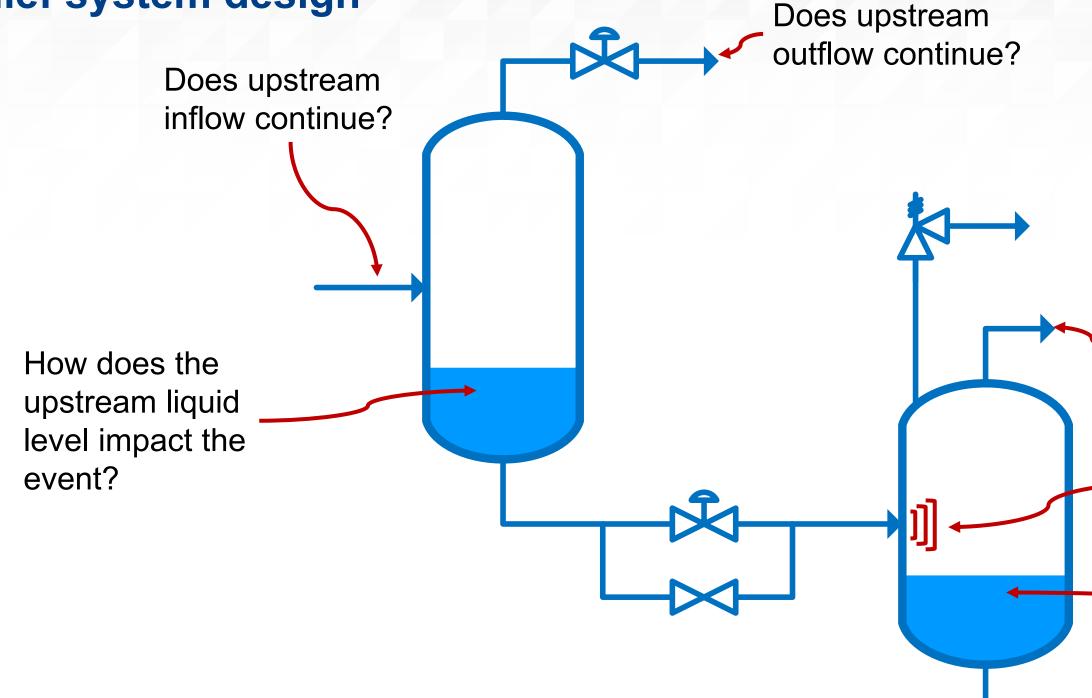
## Vapor breakthrough is a complex, dynamic scenario with many elements to consider in relief system design



Source: ioMosaic Corporation



### Vapor breakthrough is a complex, dynamic scenario with many elements to consider in relief system design



Source: ioMosaic Corporation

Does downstream vapor outflow continue?

Could high pressure surges occur downstream?

Does downstream liquid outflow continue? How does the downstream liquid level impact the event?



### Vapor breakthrough is a complex, dynamic scenario with many elements to consider in relief system design

How does the phase at the upstream vessel bottoms change throughout the relief event?

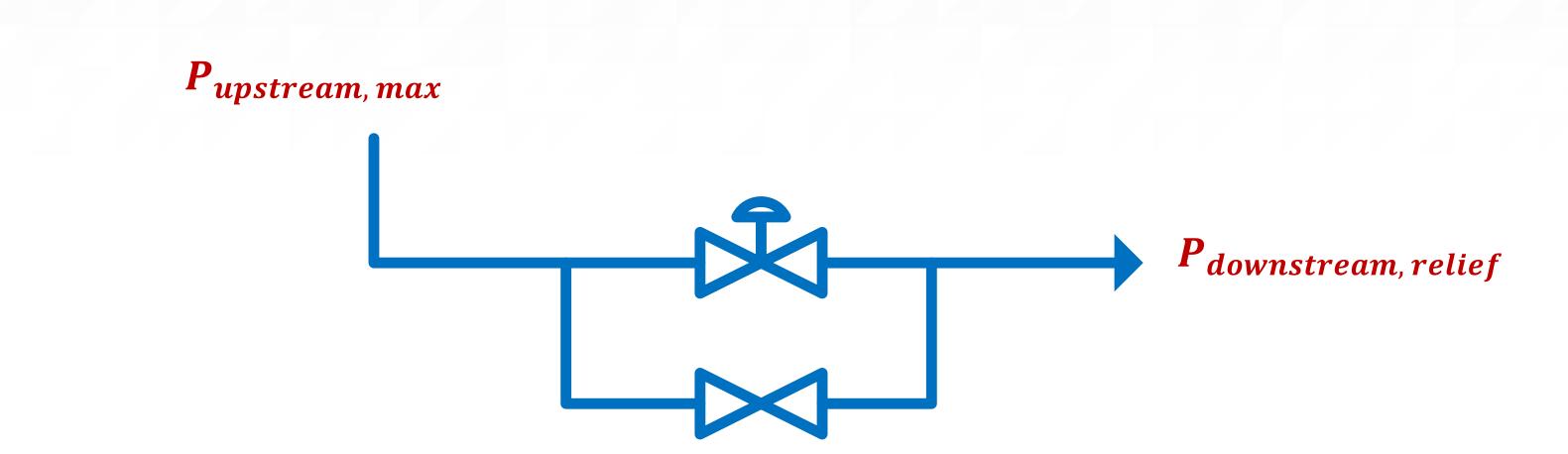
Source: ioMosaic Corporation

What is the fluid phase at the relief system inlet piping?



Steady state relief system sizing methodologies for vapor breakthrough

## Steady state methodology for vapor breakthrough sizing are often used for a conservative relief sizing

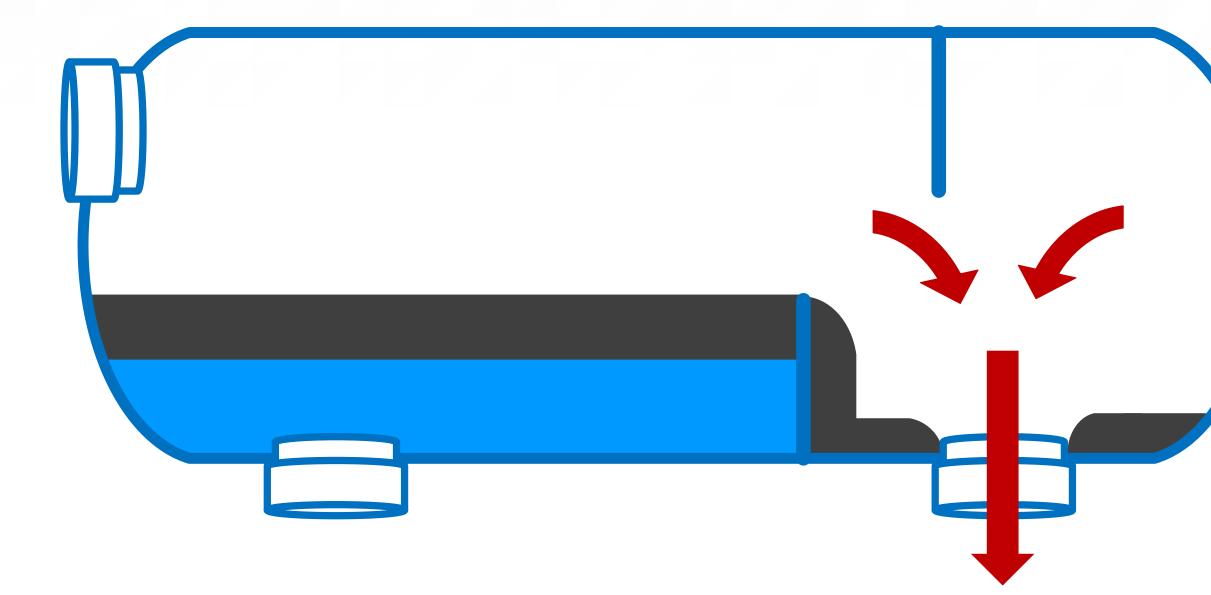


The relief requirement is typically determined with hydraulic calculations

Source: ioMosaic Corporation



## 100% vapor may still break through even if liquid remains in the upstream vessel, so be cautious crediting two-phase flow



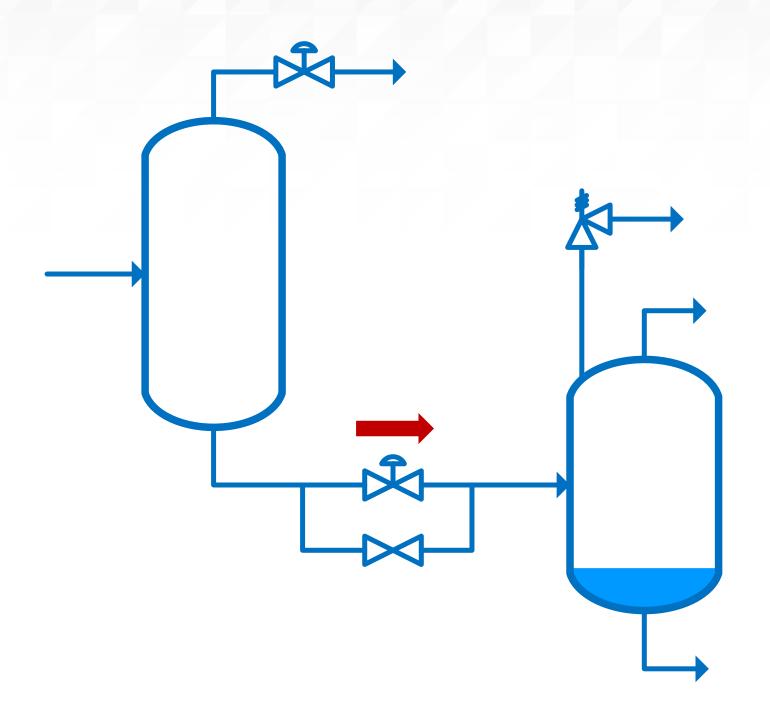
Source: ioMosaic Corporation

# 100% vapor may still break through due to:

- Sloshing liquid
- High vapor velocity
- Complex internal geometries



### 1. The liquid partially fills the downstream vessel



- nozzle)

Source: ioMosaic Corporation

© ioMosaic Corporation

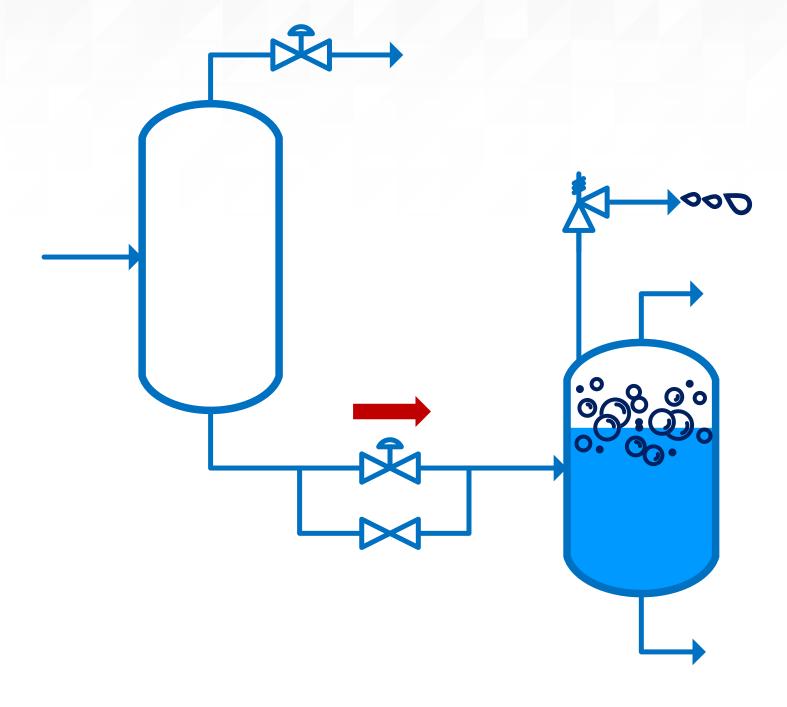


The downstream liquid level is low (usually below the inlet

### Complete vapor/liquid disengagement occurs The relief valve discharges vapor only



2. The liquid significantly fills the downstream vessel

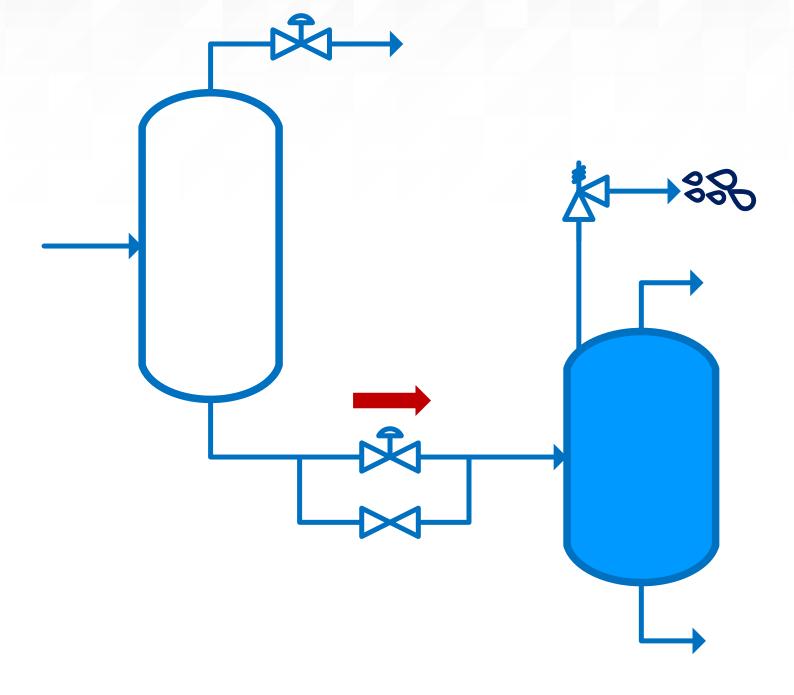


Source: ioMosaic Corporation

The downstream liquid level is significantly high (above inlet nozzle, but not filled) Partial vapor/liquid disengagement may occur The relief fluid is expected to be 2-phase



#### 3. The liquid overfills the downstream vessel



- amount of liquid

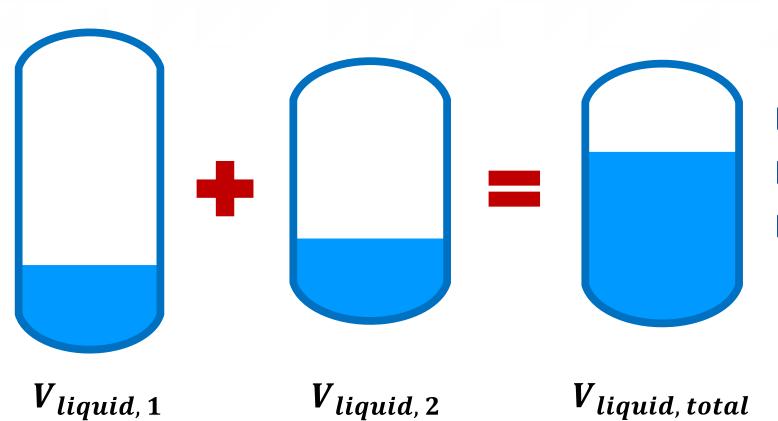
Source: ioMosaic Corporation

© ioMosaic Corporation

## The downstream vessel becomes liquid full Limited vapor/liquid disengagement may occur The relief fluid is expected to contain a significant



### The resulting downstream liquid level can be calculated with a simple volume balance



 $V_{liquid, 1} + V_{liquid, 2} = V_{liquid, total}$ 

- Flow may continue
- Flashing of liquid to vapor may occur

Source: ioMosaic Corporation

© ioMosaic Corporation

However, this methodology has limitations:

For accuracy, use a **dynamic** analysis!



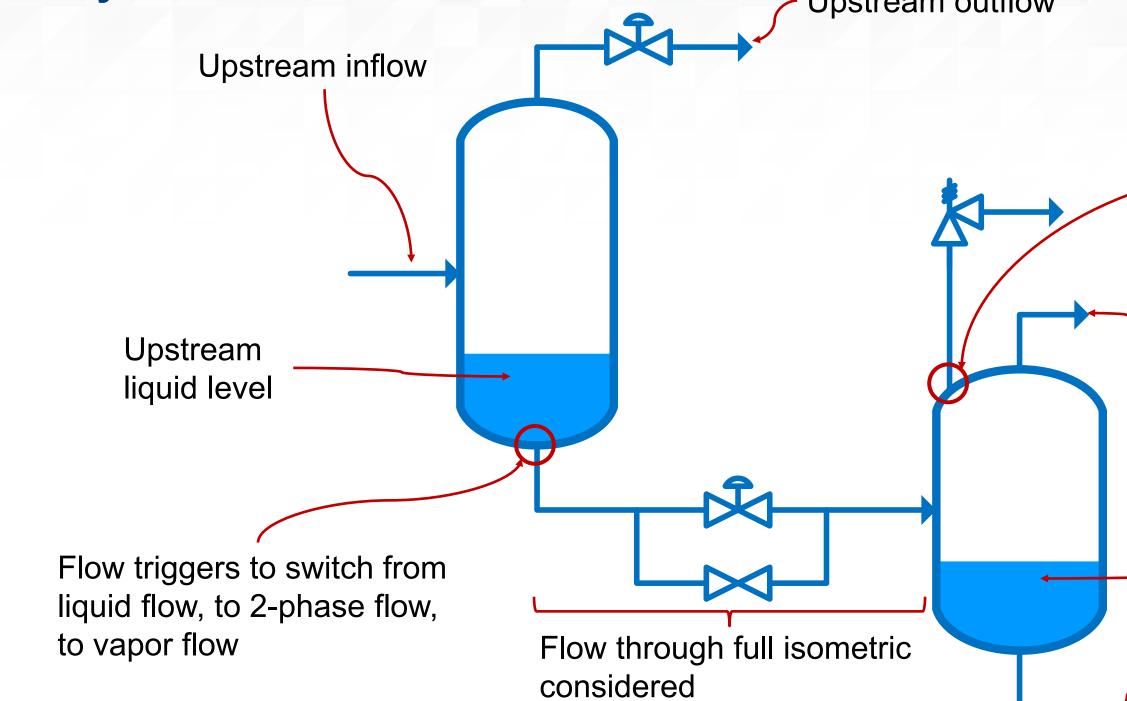
#### **Considerations when setting up the model**

- Process Safety Office<sup>®</sup> SuperChems<sup>™</sup> was used to model the scenario with lumped dynamic modelling to account for changing vessel, flow and incorporation of DIERS coupling equations
- Which flows continue, which stop?
- When does flow from upstream transition from 100% liquid flow?
- What is the relief fluid phase?
- What is the worst-case operating condition?

Source: ioMosaic Corporation



#### Dynamic modelling of vapor breakthrough can capture many more phenomena than steady state calculation methods Upstream outflow



Source: Melhem, G.A. (2017), The Anatomy of Liquid Displacement and High-Pressure Fluid Breakthrough. ioMosaic Corporation.

**DIERS** coupling equations for disengagement

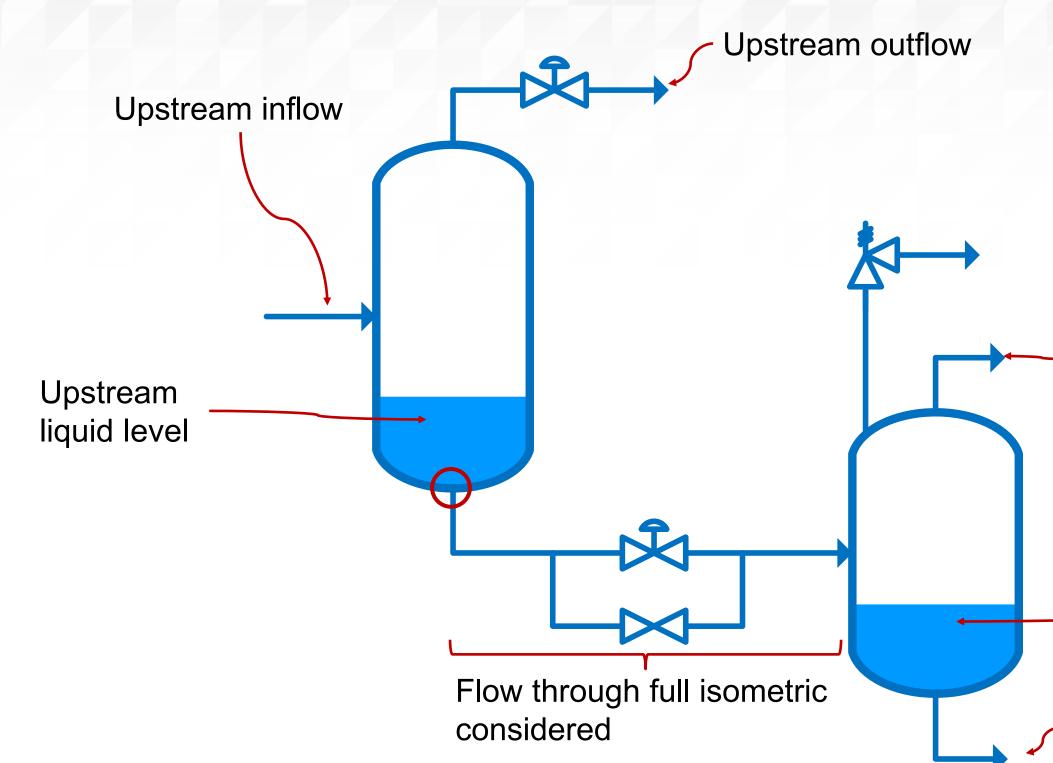
Downstream outflow

Downstream liquid level

Downstream liquid outflow



### The dynamic inflows, outflows, and liquid levels should be included



Source: Melhem, G.A. (2017), The Anatomy of Liquid Displacement and High-Pressure Fluid Breakthrough. ioMosaic Corporation.

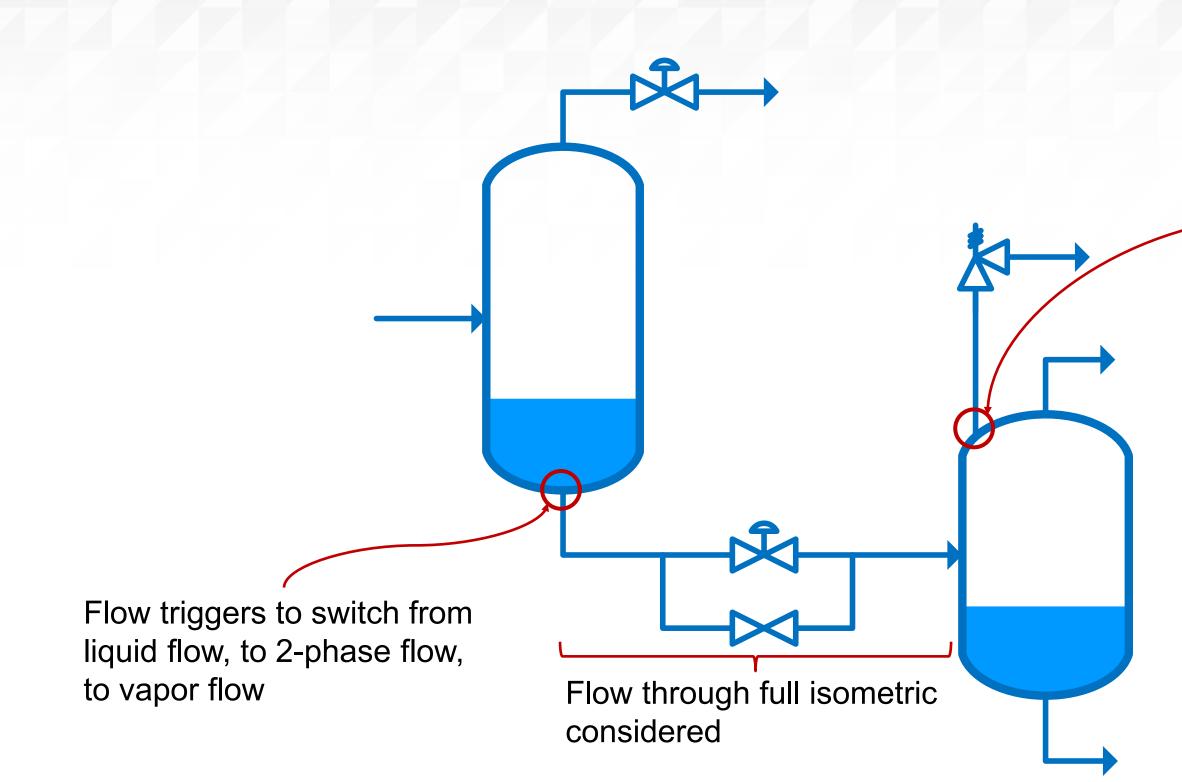
Downstream outflow

Downstream liquid level

Downstream liquid outflow



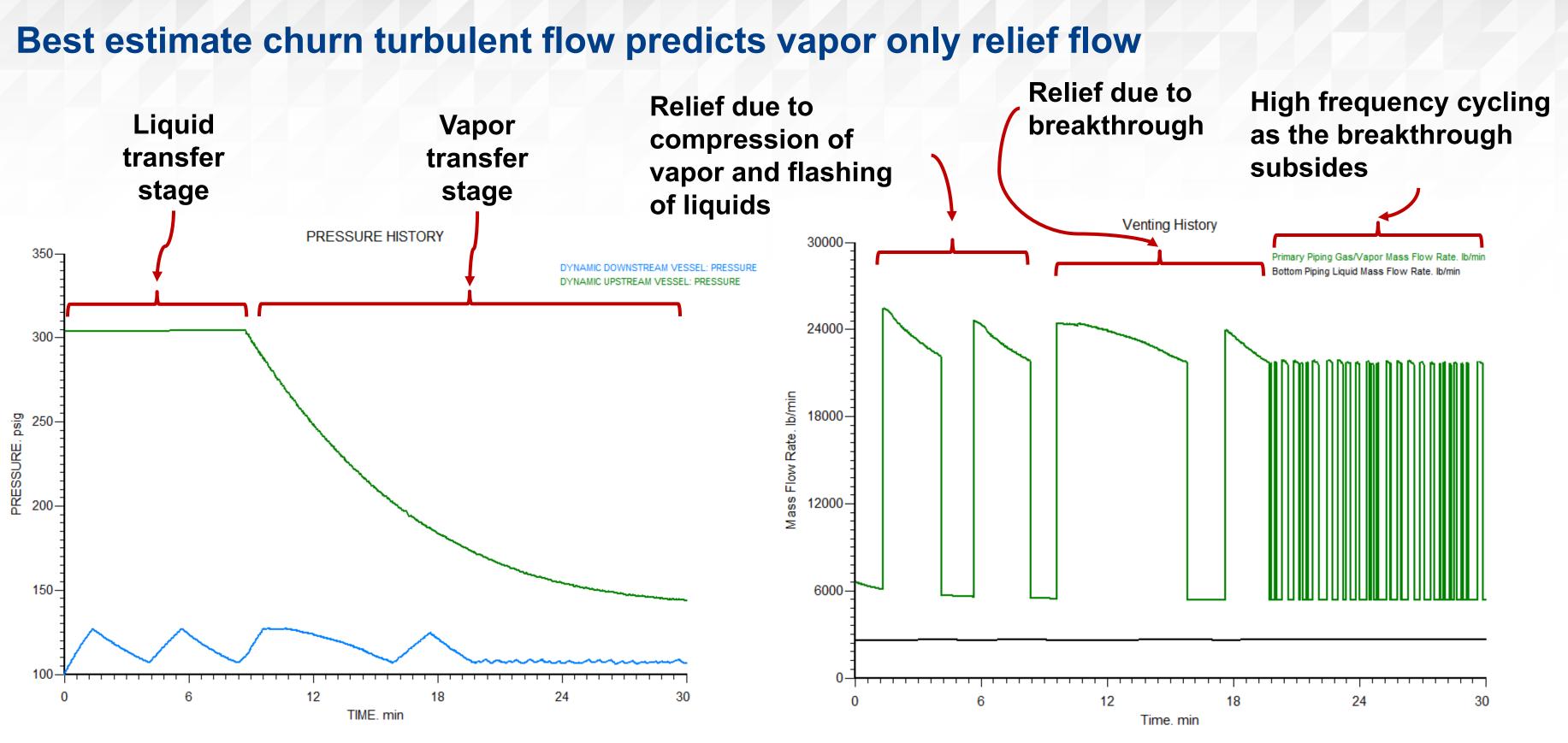
It is important to consider the phase of the flow leaving each vessel



Source: Melhem, G.A. (2017), The Anatomy of Liquid Displacement and High-Pressure Fluid Breakthrough. ioMosaic Corporation.

DIERS coupling equations for disengagement

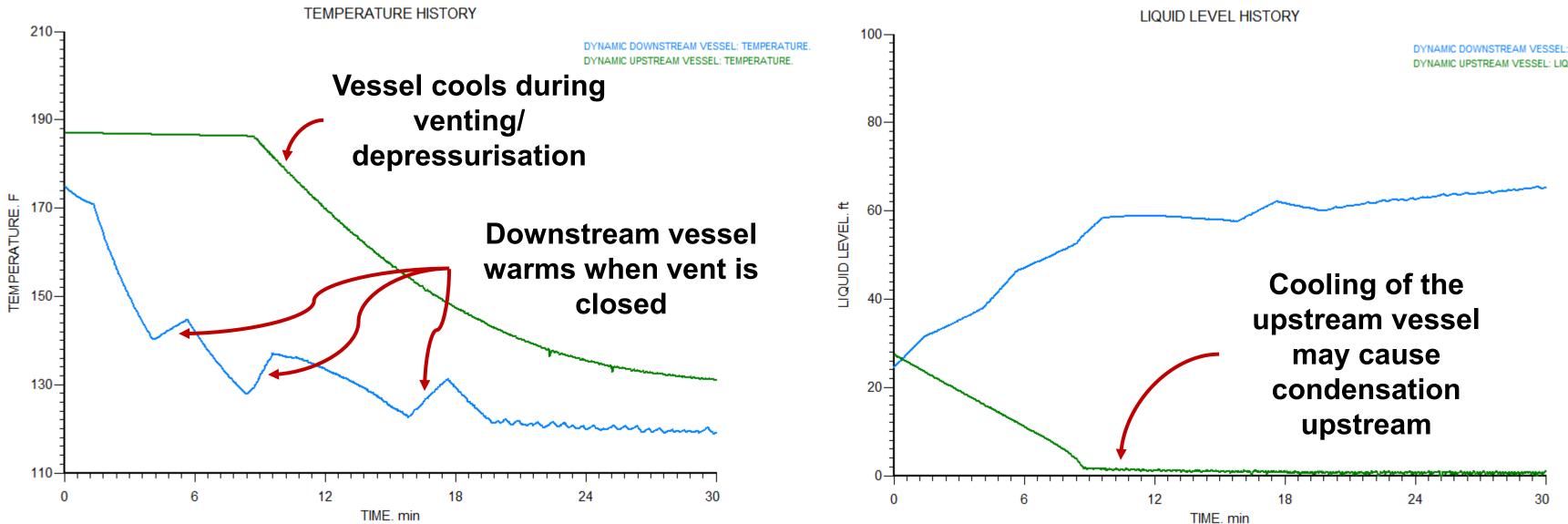




Source: ioMosaic Corporation and Process Safety Office<sup>®</sup> SuperChems™



### Dynamic results also give interesting insight into the dynamic temperature and liquid volumes



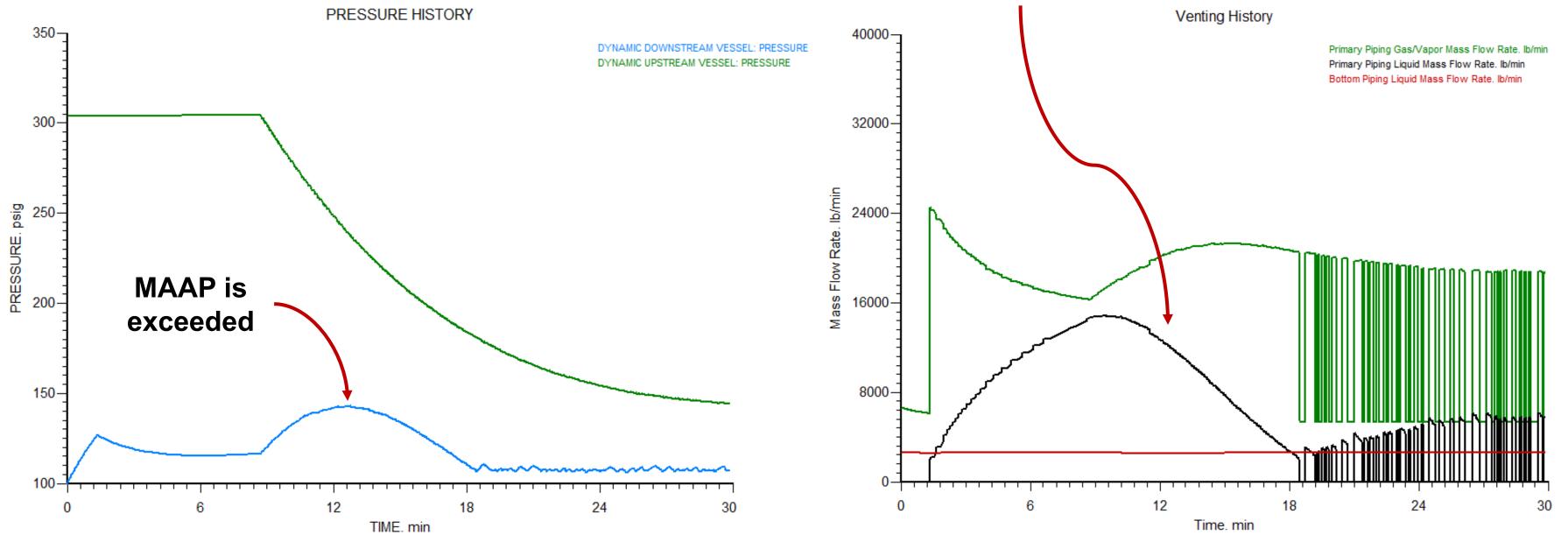
Source: ioMosaic Corporation and Process Safety Office<sup>®</sup> SuperChems™

DYNAMIC DOWNSTREAM VESSEL: LIQUID HEIGH DYNAMIC UPSTREAM VESSEL: LIQUID HEIGH



# Best estimate bubbly flow predicts 2-phase relief, which hinders effective depressurisation in the downstream system

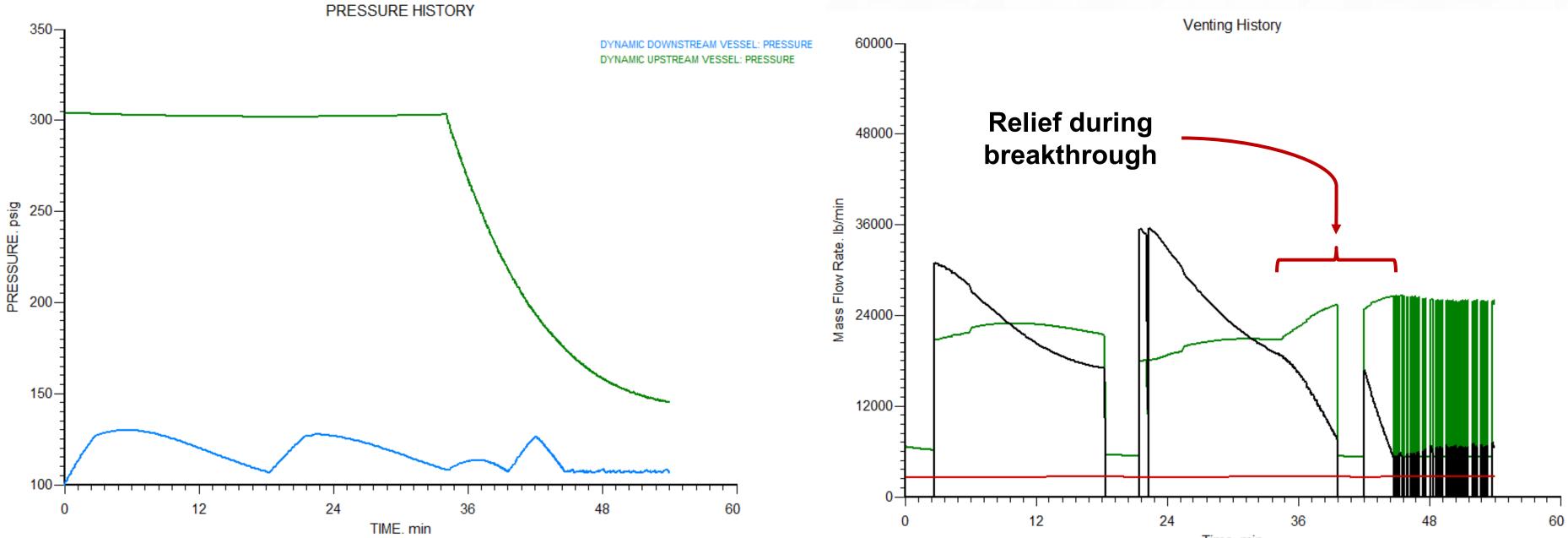
## Significant liquid relief is predicted



Source: ioMosaic Corporation and Process Safety Office<sup>®</sup> SuperChems™



## Higher starting liquid levels result in significantly more liquid relief due to less complete disengagement for best estimate churn turbulent flow

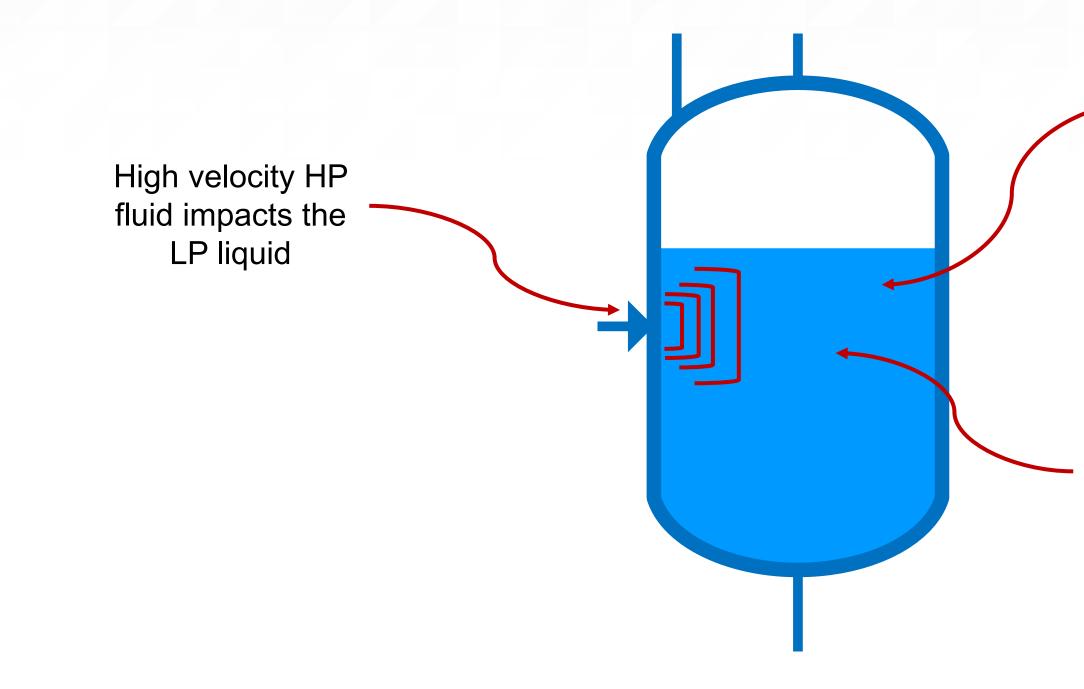


Source: ioMosaic Corporation and Process Safety Office<sup>®</sup> SuperChems™

Time. min

ioMosaic<sup>®</sup> 23

High pressure surges should also be considered especially when the downstream liquid level is high, and the pressure differential is large



Source: ioMosaic Corporation

Low velocity LP liquid

The maximum pressure loading, and shock duration should be determined



## Dynamic simulation of vapor breakthrough can give us useful insights into the anatomy of the relief event

- Calculate more accurate relief requirements
- Capture important phenomena

#### However, be careful!

- Model the worst-case scenario
- Trial multiple modes of operation

Source: ioMosaic Corporation



#### Conclusions

- Steady state methods are the most conservative and simple approach
- Remember to consider the possibility of 2-phase relief flow and overfilling downstream
- Dynamic models can provide greater insight and more accurate sizing for vapor breakthrough scenarios
- Ensure the worst-case scenario is captured



### For more information, please contact

Daniel Wilkes, Consultant wilkes.d.uk@ioMosaic.com

ioMosaic International Limited 16-18 Queen Square BATH BA1 2HN +44 (0)1225 530510

www.ioMosaic.com sales@ioMosaic.com





### **About ioMosaic Corporation**

Through innovation and dedication to continual improvement, ioMosaic has become a leading provider of integrated process safety and risk management solutions. ioMosaic has expertise in a wide variety of areas, including pressure relief systems design, process safety management, expert litigation support, laboratory services, training, and software development.

ioMosaic offers integrated process safety and risk management services to help you manage and reduce episodic risk. Because when safety, efficiency, and compliance are improved, you can sleep better at night. Our extensive expertise allows us the flexibility, resources, and capabilities to determine what you need to reduce and manage episodic risk, maintain compliance, and prevent injuries and catastrophic incidents.

Our mission is to help you protect your people, plant, stakeholder value, and our planet. For more information on ioMosaic, please visit: www.ioMosaic.com

